



EKSERJİ 2024



EKSERJİ VE UYGULAMALARI YAZ KURSU  
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# Sistemlerin Enerji ve Ekserji Analizi: Uygulamalar

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Function Information

Math and string functions  
 Thermophysical properties  
 Heat Transfer & Fluid Flow  
 Mechanical Design  
 Component Library

EES library routines  
 External routines

Real fluids  
 AirH2O  
 Brines  
 TPSX  
 Ideal gases  
 NASA  
 Incompressible

Function Info

Fluid Info

AcentricFactor	Air
CompressibilityFactor	Ar
Conductivity [W/m-K]	C2H2
Cp [kJ/kg-K]	C2H4
Cv [kJ/kg-K]	C2H5OH
Density [kg/m3]	C2H6
Dipole [debye]	C3H8
ek_LJ [K]	C4H10
Enthalpy [kJ/kg]	C5H12
Enthalpy formation [kJ/kg]	CSH14

Independent Properties

Temperature [C]

Ex: `h[0]=Enthalpy(Air,T=T[0])` [0]

Paste Done

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Thermophysical Functions

- ? ACENTRICFACTOR
- ? COMPRESSIBILITYFACTOR
- ? CONDUCTIVITY
- ? CP
- ? CV
- ? DENSITY
- ? DEWPOINT
- ? DIPOLE
- ? EK\_LJ
- ? ENTHALPY
- ? ENTHALPY\_FORMATION
- ? ENTHALPY\_FUSION
- ? ENTHALPY\_VAPORIZATION
- ? ENTROPY
- ? FREEZINGPT
- ? FUGACITY
- ? HenryConstant\_Water
- ? HIGHERHEATINGVALUE
- ? HUMRAT
- ? INTENERGY
- ? ISENTROPICEXPONENT
- ? ISOTHERMALCOMPRESS
- ? ISIDEALGAS
- ? KINEMATICVISCOSITY
- ? LOWERHEATINGVALUE
- ? MASSFRACTION
- ? MOLARMASS
- ? MOLARMASS\_SOLN
- ? NORMALBOILINGPT
- ? PHASES
- ? PRANDTL
- ? PRESSURE

## ENTHALPY

ENTHALPY [J/kg, J/kmol, kJ/kg, kJ/kmol, Btu/lbm Btu/lbmol] returns the specific enthalpy of a specified substance. The value and units of the returned value depends on the [Unit System](#) setting. The exact form of the enthalpy function depends on the substance and independent variable(s) selected. Substances that obey the ideal gas law, such as air, require a single argument in addition to the substance name (temperature or internal energy) whereas real fluid substances, e.g., Steam and CarbonDioxide, will always require two independent variables.

The specific enthalpy of [incompressible substances](#) is a function of only temperature and pressure since  $h=u+Pv$ . Both temperature and pressure must be the provided as arguments, in addition to the substance name.

For AirH2O, three arguments are required. One of these arguments must be total pressure (P). The remaining two can be any of the following: temperature (T), internal energy (U), relative humidity (R), humidity ratio (W), wetbulb (B), or dewpoint (D). Note also that for substance AirH2O (psychrometrics), the specific enthalpy returned by this function is the enthalpy of the air and water vapor mixture per unit mass of dry air.

The reference state upon which the value of enthalpy is based varies with the substance.

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- Academic License (\$2500) (Includes one year of Academic Update Service)

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- Professional, >12 and <48 months past expiration (\$480)

Detaylor: <https://fchartsoftware.com/ees/>

```

X_1=1 {will display as X with a subscript 1}
X_infinity=2 { will display as X with subscript ?}
X_bar=3 {will display with a bar centered above the X}
X_dot=4 {will display with a dot centered above the X}
X_ddot=5 {will display with a double-dot centered above the X}
X_hat=6 {will display with a hat (^) centered above the X}
X_tilde=7 {will display with a tilde (~) center above the X}

X|minus=8 {will display as X superscript -}
X|o=9 {will display as X superscript o}
X|plus=10 {will display as X superscript+}
X|star=11 {will display as X*}

X_prime=12 {will display as X'}
X_dprime=13 {will display as X''}
X_tprime=14 {will display as X'''}

```

B|W US Line: 16 Char: 35 Wrap: On Insert Caps Lock: Off SI K Pa J mass rad Warnings: On Unit Chk: On

```

Solution
Main
Unit Settings: SI K Pa J mass rad

X1 = 1           X̄ = 3
Ẍ = 5             Ẋ = 4
X'' = 13          X̂ = 6
X∞ = 2          X' = 12
X̃ = 7             X''' = 14
X- = 8          Xo = 9
X+ = 10        X* = 11

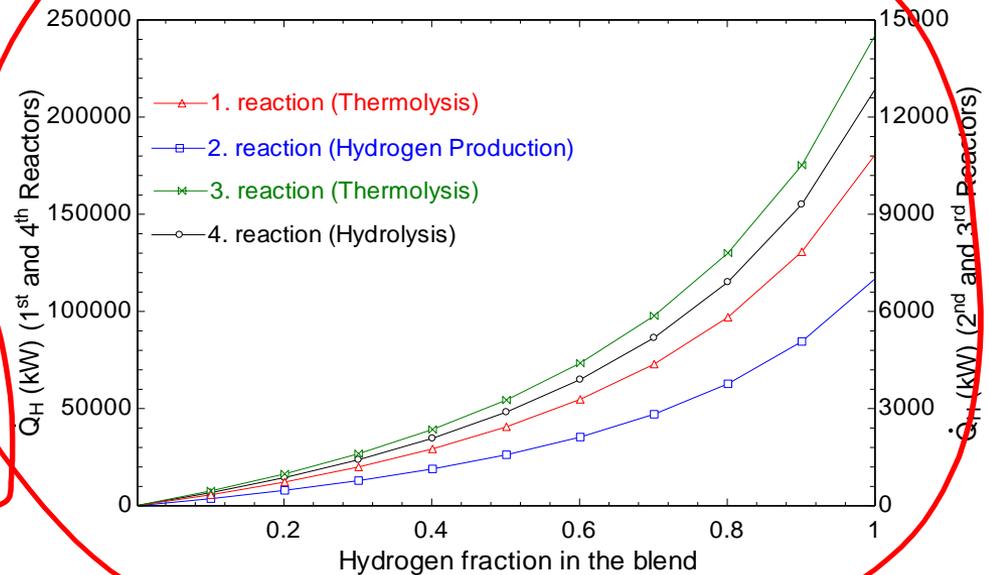
No unit problems were detected.
Compilation time = 21 ms Calculation

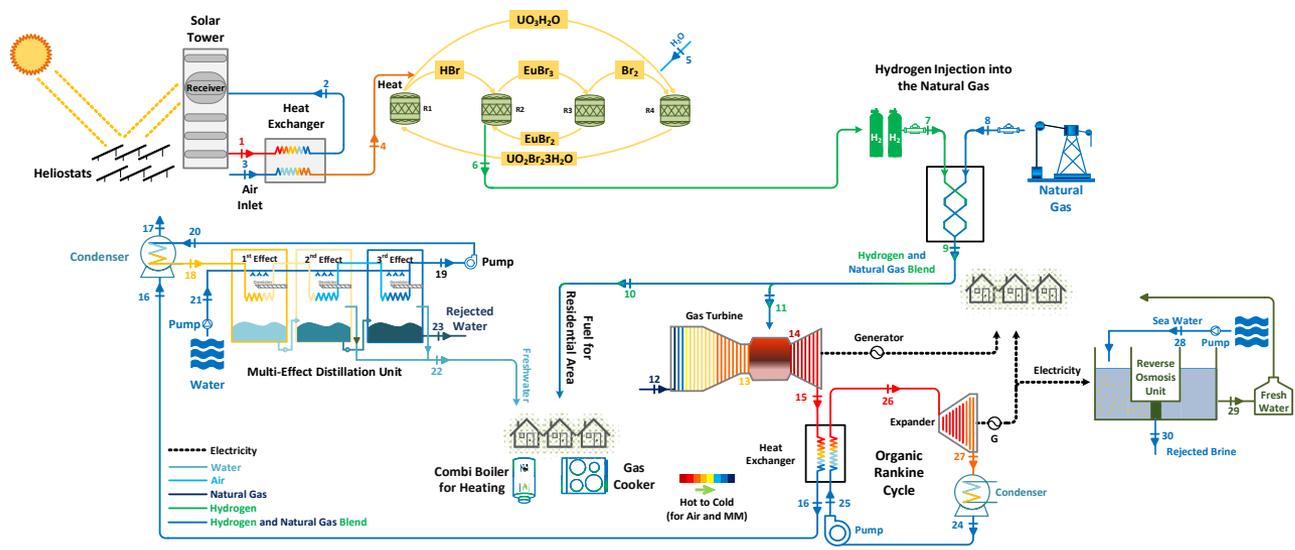
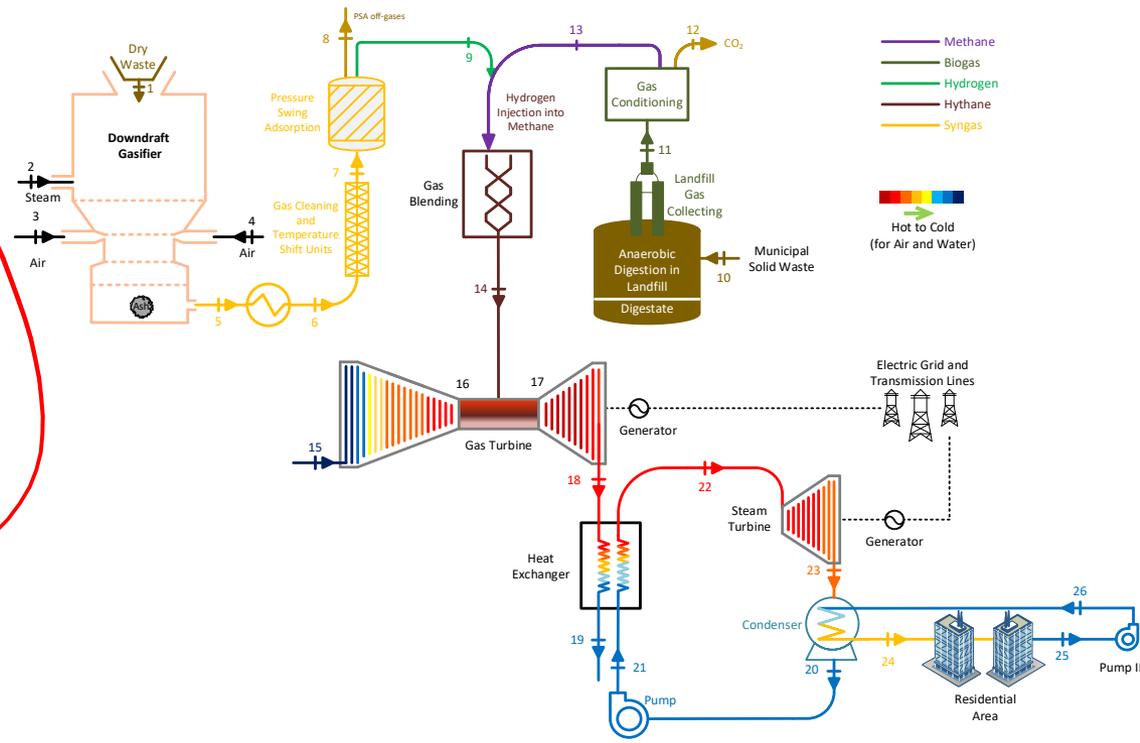
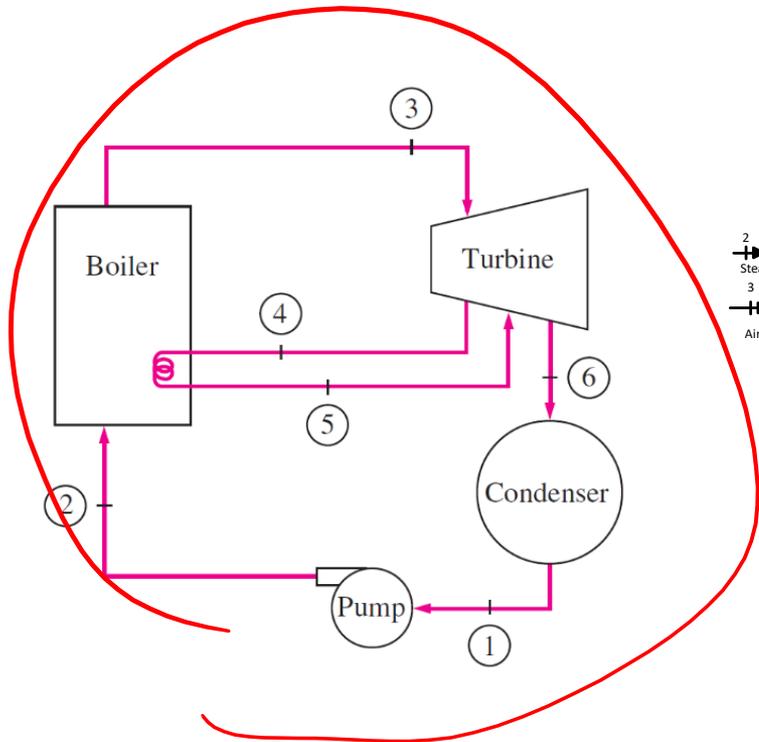
```

EES Variable Name	Upper Case Symbol	Lower Case Symbol	EES Variable Name	Upper Case Symbol	Lower Case Symbol
ALPHA	α	α	MU	μ	μ
BETA	β	β	NU	ν	ν
CHI	χ	χ	THETA	θ	θ
DELTA	Δ	δ	RHO	ρ	ρ
EPSILON	ε	ε	SIGMA	Σ	σ
PHI	Φ	φ	TAU	τ	τ
gamma	Γ	γ	UPSILON	υ	υ
ETA	η	η	OMEGA	Ω	ω
IOTA	ι	ι	XI	Ξ	ξ
JTHETA	ϑ	φ	PSI	Ψ	ψ
KAPPA	κ	κ	ZETA	Ζ	ζ
LAMBDA	Λ	λ			

	1	2	3	4	5	6	7	8	9	10	11	12	13
	$f$ [-]	$f_{mass}$ [-]	$f_{Air}$ [-]	$f_{CH4}$ [-]	$f_{CO2}$ [-]	$f_{exhaust,gases}$ [-]	$f_{H2}$ [-]	$f_{H2O}$ [-]	$f_{N2}$ [-]	$m_1$ [kg/s]	$m_{10}$ [kg/s]	LHV <sub>hythane</sub> [kJ/kg]	LHV <sub>hythane,v</sub> [kJ/m <sup>3</sup> ]
Run 31	0.6	0.1586	5.263	0.4	0.4	5.963	0.6	1.4	4.163	0.2677	0.848	61113	1881
Run 32	0.62	0.1701	5.12	0.38	0.38	5.81	0.62	1.38	4.05	0.2834	0.8255	61920	1836
Run 33	0.64	0.1826	4.976	0.36	0.36	5.656	0.64	1.36	3.936	0.3	0.8018	62791	1790
Run 34	0.66	0.1961	4.832	0.34	0.34	5.502	0.66	1.34	3.822	0.3173	0.7769	63735	1745
Run 35	0.68	0.2107	4.689	0.32	0.32	5.349	0.68	1.32	3.709	0.3357	0.7507	64760	1700
Run 36	0.7	0.2267	4.545	0.3	0.3	5.195	0.7	1.3	3.595	0.355	0.723	65877	1654
Run 37	0.72	0.2442	4.402	0.28	0.28	5.042	0.72	1.28	3.482	0.3754	0.6938	67099	1609
Run 38	0.74	0.2634	4.258	0.26	0.26	4.888	0.74	1.26	3.368	0.397	0.6629	68443	1564
Run 39	0.76	0.2846	4.115	0.24	0.24	4.735	0.76	1.24	3.255	0.4199	0.6301	69927	1519
Run 40	0.78	0.3082	3.971	0.22	0.22	4.581	0.78	1.22	3.141	0.4442	0.5953	71574	1473
Run 41	0.8	0.3345	3.828	0.2	0.2	4.428	0.8	1.2	3.028	0.47	0.5583	73413	1428
Run 42	0.82	0.364	3.684	0.18	0.18	4.274	0.82	1.18	2.914	0.4975	0.519	75479	1383
Run 43	0.84	0.3975	3.541	0.16	0.16	4.121	0.84	1.16	2.801	0.5269	0.4769	77817	1338
Run 44	0.86	0.4356	3.397	0.14	0.14	3.967	0.86	1.14	2.687	0.5583	0.4319	80484	1292

Last Digit in Student ID	Pressure Ratio ( $r_p$ )	Gas Turbine Inlet Temp. ( $T_4$ ) (K)	Isentropic efficiency of gas turbine ( $\eta_{GT}$ ) (%)	Steam Turbine Inlet Pressure ( $P_5$ ) (MPa)
0	7	1200	75	8
1	8	1250	76	9
2	9	1300	77	10
3	10	1350	78	11
4	11	1400	79	12
5	12	1450	80	13
6	13	1500	81	14
7	14	1550	82	15
8	15	1600	83	16
9	16	1650	84	17





# Organic Rankine cycle plant

